



Supplement of

Simulating the feedback between corrosive gas generation and water availability for the evaluation of radionuclide mobility in the context of radioactive waste disposal

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Simulating the feedback between corrosive gas generation and water availability for the evaluation of radionuclide mobility in the context of radioactive waste disposal

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The importance of gas generation for radioactive waste disposal

- May affect the mobility of dissolved and volatile radionuclides through changes in phase saturation
- May affect mobility of dissolved and volatile radionuclides through changes in geochemical conditions (Eh, pH_m, etc.)
- May induce advective transport
- May affect the mechanical stability of the host rock and open up dilatant transport pathways
- + May affect the integrity of technical and geotechnical barriers



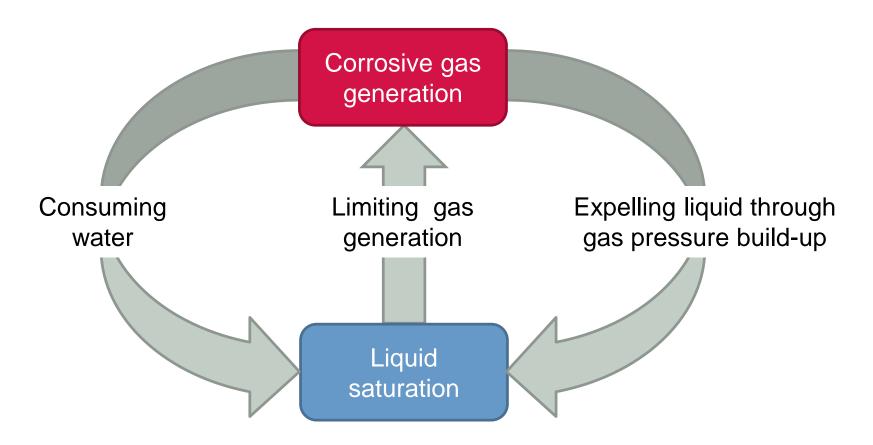


Perception of gas generation as kinetic geochemical reactions

Cellulose oxidation by molecular oxygen (c_o)	$C6H10O5 + 6 O2 \implies 5 H2O + 6 CO2$
Cellulose oxidation by nitrate (c_n)	C6H10O5 + 4.8 NO3- + 4.8 H+ => 2.4 N2 + 7.4 H2O + 6 CO2
Cellulose oxidation by sulfate reduction (c_s)	C6H10O5 + 3 SO4-2 + 6 H+ => 3 H2Sg + 5 H2O + 6 CO2
Cellulose oxidation by Fe(III) reduction (c_f)	C6H10O5 + 24 FeOOH + 7 H2O => 24 Fe(OH)2 + 6 CO2
Methane generation from cellulose (c_m)	C6H10O5 + 3 H2O => 4 H2 + 2 CH4 + 4 CO2
Plastics oxidation by molecular oxygen (p_o)	C2H4 + 3 O2 => 2 H2O + 2 CO2
Plastics oxidation by nitrate (p_n)	C2H4 + 2.4 NO3- + 2.40 H+ => 1.2 N2 + 3.2 H2O + 2 CO2
Plastics oxidation by sulfate reduction (p_s)	C2H4 + 1.5 SO4-2 + 3 H+ => 1.5 H2S + 2 H2O + 2 CO2
Plastics oxidation by Fe(III) reduction (p_f)	C2H4 + 12 FeOOH + 4 H2O => 12 Fe(OH)2 + 2 CO2
Methane generation from plastics (p_m)	C2H4 + 2.666667 H2O => 3.333333 H2 + 0.6666667 CH4 + 1.333333 CO2
Hydrogen oxidation by Fe(III) reduction (h_o)	H2 + 2 FeOOH => 2 Fe(OH)2
Hydrogen oxidation by CO2 reduction (h_m)	H2 + 0.25 CO2 => 0.25 CH4 + 0.5 H2O
Hydrogen oxidation by sulfate reduction (h_s)	H2 + 0.25 SO4-2 + 0.5 H+ => 0.25 H2S + 1 H2O
Aerobe corrosion of C-steel (cs_o)	Fe(0) + 0.5 H2O + 0.75 O2 => 1 FeOOH
Anaerobe corrosion of C-steel (cs_h)	Fe(0) + 1.333333 H2O => 1.333333 H2 + 0.333333 Fe3O4
Reduction of Fe(III) with C-Steel (cs_r)	0.5 Fe(0) + 1 FeOOH => 0.5 H2 + 0.5 Fe3O4
Aerobe corrosion of stainless steel (ss_o)	Fe(0) + 0.5 H2O + 0.75 O2 => 1 FeOOH
Anaerobe corrosion of stainless steel (ss_h)	Fe(0) + 1.333333 H2O => 1.333333 H2 + 0.333333 Fe3O4
Reduction of Fe(III) with stainless steel (ss_r)	0.5 Fe(0) + 1 FeOOH => 0.5 H2 + 0.5 Fe3O4
Oxidation of Fe(II) with hydrogen (Schikorr reaction) (fe_sch)	Fe(OH)2 => 0.333333 H2 + 0.333333 Fe3O4 + 0.6666667 H2O
Iron sulfide precipitation (fe_sul)	H2Sg + 1 Fe(OH)2 => 2 H2O + 1 FeS
Anaerobe corrosion of aluminium (al_h)	AI(0) + 4 H2O => 1.5 H2 + 1 AI(OH)4- + 1 H+



Feedback of corrosive gas generation and water availability







- Xu et al. (2008): Corrosion-induced gas generation in a nuclear waste repository: Reactive geochemistry and multiphase flow effects. Applied Geochemistry, 23, 3423– 3433. doi:<u>10.1016/j.apgeochem.2008.07.012</u>
- Croisé et al. (2011): Impact of water consumption and saturation-dependent corrosion rate on hydrogen generation and migration from an intermediate-level radioactive waste repository. Transport in Porous Media, 90, 59–75. doi:<u>10.1007/s11242-011-9803-0</u>
- Leupin et al. (2016): An assessment of the possible fate of gas generated in a repository for low- and intermediate-level waste. Nationale Genossenschaft f
 ür die Lagerung radioaktiver Abf
 älle (NAGRA), Nagra Working Report, NTB 16-05.
- Huang et al. (2021): Two-phase transport in a cemented waste package considering spatio-temporal evolution of chemical conditions. npj Materials Degradation, 5, 4. doi:<u>10.1038/s41529-021-00150-z</u>



What's new

- Implementation in PFLOTRAN: A Massively Parallel Reactive Flow and Transport Model for Describing Surface and Subsurface Processes
- + Application to radioactive waste management in salt host rock





PFLOTRAN

- A massively parallel reactive flow and transport model for describing surface and subsurface processes
 - Multicomponent 2-Phase flow: GENERAL mode
 - 2-phase water and supercritical CO₂ flow: MPHASE mode
- + Designed *ab initio* with reactive transport capabilities
- Designed for application to salt host rock
 - Intended as replacement for several other codes currently used in the periodic performance assessment and recertification process for the WIPP
- + Developed in close cooperation with the team behind the PETSc solver suite
- Developed by consortium of Los Alamos National Lab, Oak Ridge National Lab, Pacific Northwest National Lab and Sandia National Labs
- + The code is open source; available at https://bitbucket.org/pflotran/pflotran/wiki/Home



Reaction equations

Simplified anoxic iron corrosion reaction with Magnetite as corrosion product:

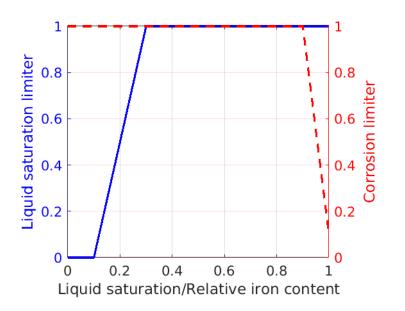
$$3Fe^{0} + 4H_{2}^{+I}O^{-II} \rightarrow (Fe^{+II}Fe_{2}^{+III})O_{4}^{-II} + 4H_{2}^{0}$$

+ Conceptualized as kinetic reaction with rate:

$$r_0 = \frac{dm_{Fe^0}}{dt} = \frac{k \cdot A \cdot \rho_{Fe^0}}{M_{Fe^0}}$$

+ Linear reduction of corrosion rate at onset:

$$r_{1} = r_{0} \cdot \begin{cases} 9.1 - 9 \cdot m_{Fe} & 0.9 \cdot m_{Fe_{0}^{0}} \leq m_{Fe} < m_{Fe_{0}^{0}} \\ 1 & m_{Fe} \leq 0.9 \cdot m_{Fe_{0}^{0}} \end{cases}$$



+ Linear reduction of corrosion rate with decreasing liquid content (similar reduction with depletion of iron inventory):

$$r_{2} = r_{1} \cdot \begin{cases} 0 & S_{l} \leq S_{l,1} \\ \frac{S_{l} - S_{l,1}}{S_{l,2} - S_{l,1}} & S_{l,1} < S_{l} < S_{l,2} \\ 1 & S_{l} \geq S_{l,2} \end{cases}$$

+ Differentiation of 3 different iron pools with different Fe_0^0 , different A_0 and different k



Implementation in PFLOTRAN

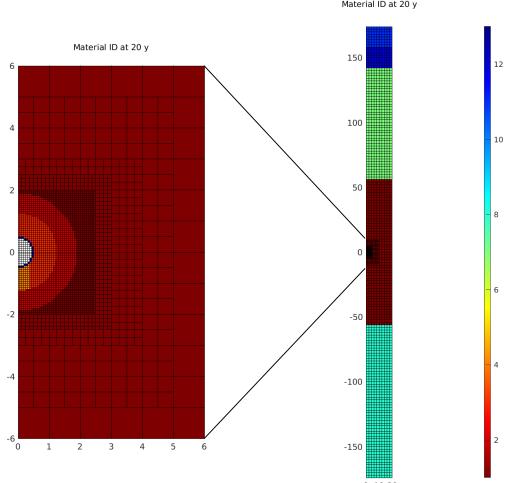
- Using object-oriented coding provisions with encapsulation, inheritance, and polymorphism in PFLOTRAN for user-defined source/sink terms: SRCSINK_SANDBOX
- SRCSINK_SANDBOX: Fortran 90 class with access to all important process variables
- Adapting directly the residuals in the numerical solution for the gas and liquid phases as well as temperature
- Output of process variables to result files (HDF5, ASCII etc.)
- Direct visualization in Tecplot, Vislt and ParaView

MAW-GAS_GENERATION	
CELL_ID 4801	
WASTE1_IRON	# kmol/m³
WASTE1_CORROSION_RATE	# kmol/m³/s
WASTE2_IRON	# kmol/m³
WASTE2_CORROSION_RATE	# kmol/m³/s
DRUM_IRON	# kmol/m³
DRUM_CORROSION_RATE	#kmol/m³/s
WC_LIM 0.3	
WC_MIN 0.1	
END	



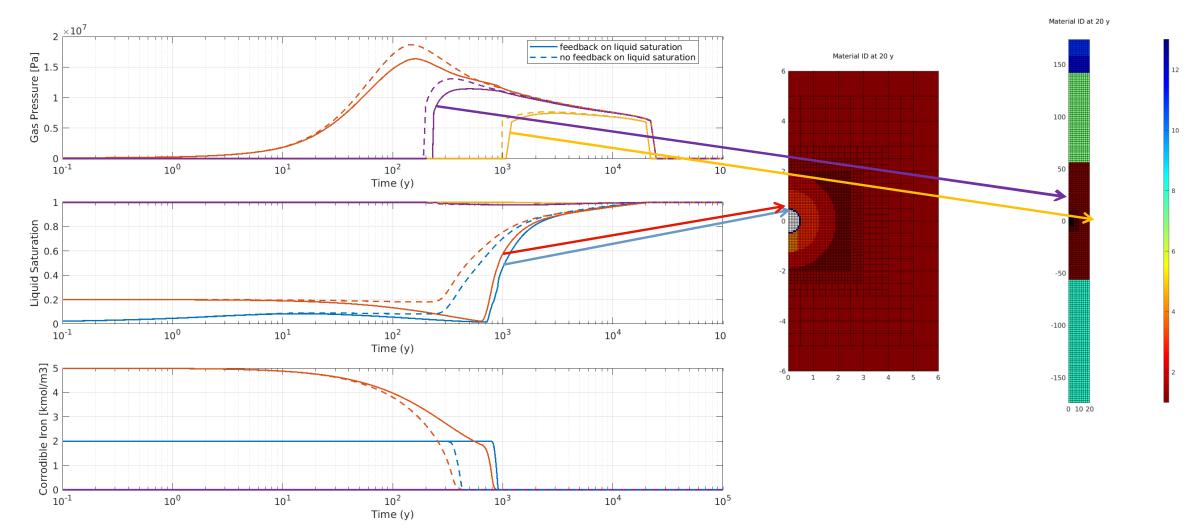
Application example

- Simulation modified on the basis of benchmark calculations between TOUGH2 and PFLOTRAN
- Original simulations published in Namhata, A., Li, C., Papafotiou, A.: Model-based assessment of repository induced effects in the vicinity of repositories for SF/HLW. In Management of Spent Fuel from Nuclear Power Reactors, IAEA, International Atomic Energy Agency (IAEA). ISBN 0074-1884
- + Emplacement tunnel in clay host rock with
 - Steel canister and iron reinforcement
 - 2 types of Bentonite backfill
 - Stylized EDZ
 - Confining units
 - Rectangular 2D grid with octree grid refinement



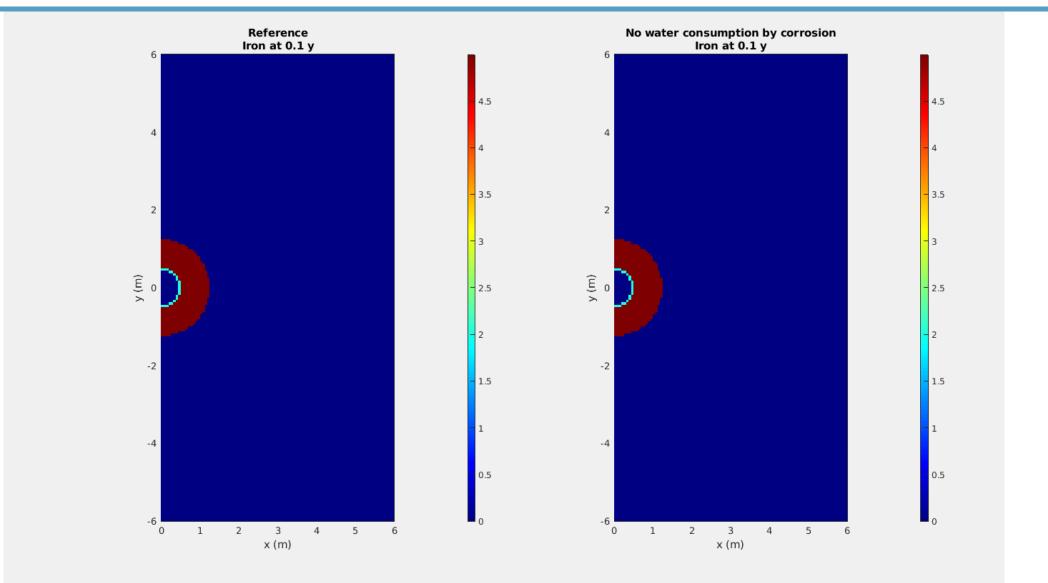


Comparison of model results with and without water consumption for different locations





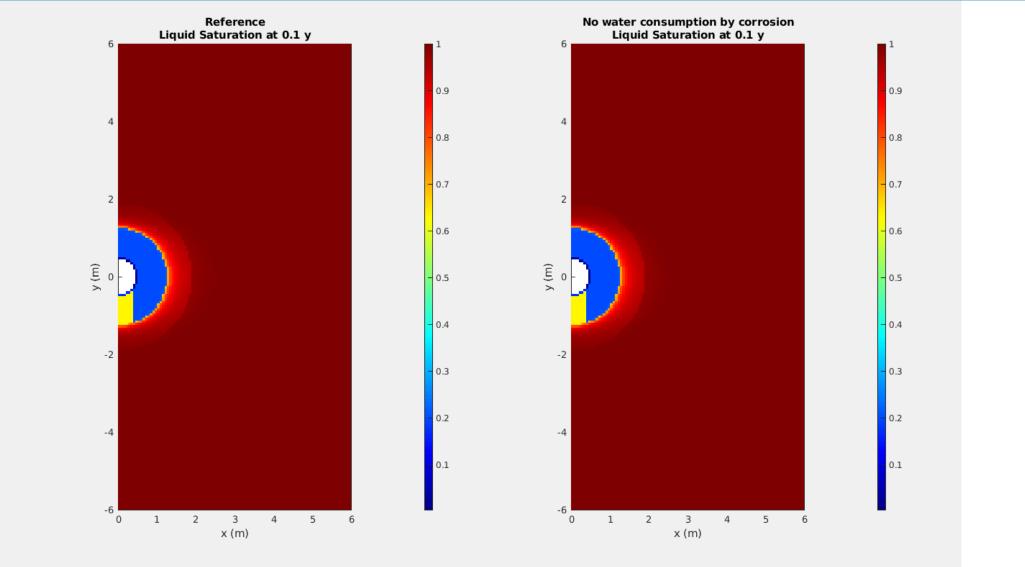
Comparison of model results: Evolution of corrodible iron content



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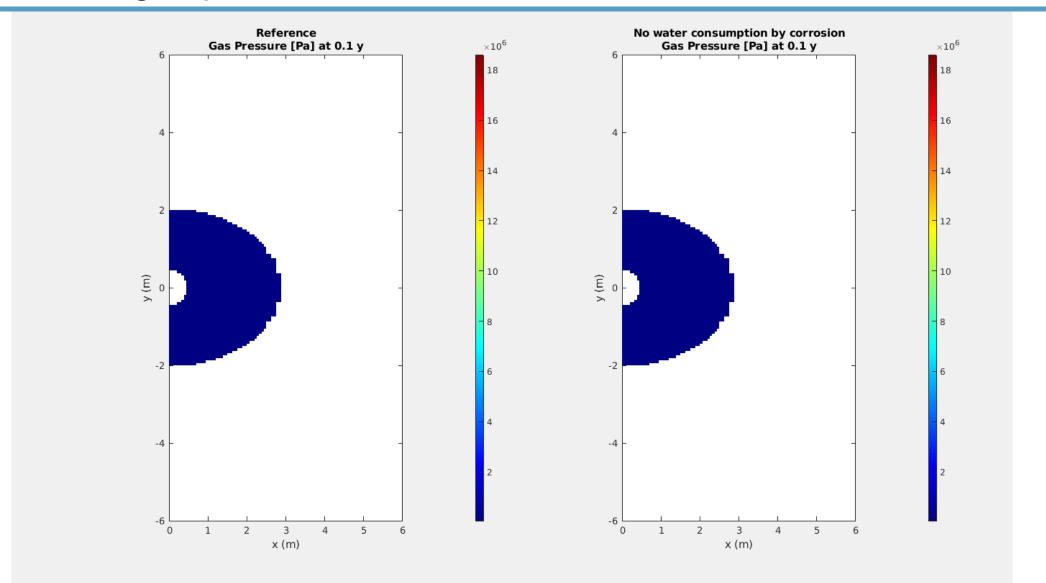
Comparison of model results: Evolution of liquid saturation



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Comparison of model results: Evolution of gas pressure





Summary

- We have shown the importance to consider also water as educt / product of gas generating reactions in the context of 2-phase flow simulations
- We have detailed the implementation of water consuming anoxic corrosion into the flow and reactive transport simulator PFLOTRAN
- + We have given an application example for a generic repository layout
- + For further information, send an e-mail to:

I.wissmeier@csd.ch

Thank you for your attention!

